

## The Study of MgO and/or ZrO<sub>2</sub> Modified Al<sub>2</sub>O<sub>3</sub> for CO<sub>2</sub> Adsorption

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### Abstract

Alumina (Al<sub>2</sub>O<sub>3</sub>) is widely used as a sorbent in CO<sub>2</sub> adsorption and as a catalyst support in CO<sub>2</sub> utilization. For this application, the CO<sub>2</sub> adsorption ability is the most important property to be improved. Thus, this work presents the idea to modify the surface of a commercial alumina using an Mg-Zr mixed oxide. With this material, sites for CO<sub>2</sub> adsorption can be created by generating oxygen mobility property simultaneously with the basicity. To prove this hypothesis, alumina modified with MgO, ZrO<sub>2</sub>, or Mg-Zr mixed oxide was prepared by an incipient wetness impregnation. The physicochemical properties of the bare alumina and the alumina modified with MgO, ZrO<sub>2</sub>, or Mg-Zr mixed oxide were investigated using N<sub>2</sub> adsorption-desorption and X-ray diffraction. The achievement of oxygen mobility creation was quantitatively evaluated by O<sub>2</sub>-temperature programmed desorption measurement. The CO<sub>2</sub> adsorption performance with the distribution of basic site strength was determined by CO<sub>2</sub>-temperature programmed desorption measurements. According to the results, the highest oxygen mobility was found in the alumina modified with Mg-Zr mixed oxide, which is approximately 1.7 times that of the bare alumina. The alumina modified with Mg-Zr mixed oxide showed the highest CO<sub>2</sub> capacity by approximately 1.4 times compared to the alumina. It is because the cubic ZrO<sub>2</sub> stabilized with MgO provided the number of oxygen vacancy sites that can be filled by oxygen atoms in adsorbed CO<sub>2</sub> corresponding to the moderate and strong basic sites.

**Keywords:** Oxygen mobility, Solid adsorbent, Alumina, Carbon dioxide capture, Magnesium oxide, Zirconia

### 1 Introduction

At present, the world is facing a climate crisis due to the rising impact of global warming caused by an increase in the emission of greenhouse gases (Green House Gases (GHG)). Among many greenhouse gases, carbon dioxide (CO<sub>2</sub>) emission is considered a major problem because of the CO<sub>2</sub> accumulation in the Earth's atmosphere. In 2021, global CO<sub>2</sub> concentration reaches 415 ppm, 1.5-fold of the CO<sub>2</sub> concentration in 1750 [1]. This concentration is much higher than the safe concentration of CO<sub>2</sub> in the atmosphere (350 ppm) defined by the World Health Organization (WHO) [2]. In order not to release excess CO<sub>2</sub> into the atmosphere, there have been many researches attempts to develop technologies for this purpose.

Renewable energy technologies are considered the clean energy production derived from renewable sources such as biomass, wind, solar, and water. Their availability is still lower than the overall energy demand [3]. CO<sub>2</sub> capture utilization and storage (CCUS) is an essential emissions reduction technique that solves the problem of global warming by reducing CO<sub>2</sub> emissions [4]. CO<sub>2</sub> capture and storage is a set of technologies that capture CO<sub>2</sub> and then inject it into suitable underground storage reservoirs to prevent it from being released into the atmosphere. Rather than being stored underground, many studies utilized the captured CO<sub>2</sub> as a raw material for high value-added products. Thus, various approaches for CO<sub>2</sub> capture have been developed recently, including membrane separation, amine-based solvents, ionic liquids, and

cryogenic fractionation. However, these technologies have the problem of intensive regenerated energy consumption, and environmental corrosion problems [5]. Moreover, the difficulty of CO<sub>2</sub> separation from liquid absorbents is an obstacle to CO<sub>2</sub> utilization. To avoid this problem, the solid adsorbent for CO<sub>2</sub> capture is considered a more appropriate technique due to the easier and lower-cost separation [6].

Solid adsorbents are one of the most environmentally friendly materials involved in CO<sub>2</sub> capture and utilization technique due to their recoverability and reusability [7], [8]. The adsorbents, also known as solid sorbents, require various properties for adsorbing CO<sub>2</sub> consisting of a high specific surface area, pore structure, thermal stability, and basic surface. Adsorbents such as zeolites, carbon-based materials, metal-organic frameworks, and alkaline earth metal oxides have been studied by many works recently [9]–[11]. However, these adsorbents still showed the drawback of thermal and mechanical stability which obstruct their adsorption-regeneration cycle and commercial application.

Alumina (Al<sub>2</sub>O<sub>3</sub>) is a versatile material, which has many attractive properties including a large surface area, great thermal and mechanical stability, and acid-base surface properties. Consequently, Al<sub>2</sub>O<sub>3</sub> is commonly used as an adsorbent as well as a catalyst support. Considering the acid-basic surface properties which show a strong effect on CO<sub>2</sub> adsorption, sites on the Al<sub>2</sub>O<sub>3</sub> surface present a stronger acid than a basic [12]. As a result of the acidic nature of CO<sub>2</sub>, pure Al<sub>2</sub>O<sub>3</sub> has a low CO<sub>2</sub> adsorption capability.

According to certain works, MgO is a promising material, which has high moderate basicity and adsorption/desorption capacities at medium to high temperatures. However, it has a lower surface area and pore structure than Al<sub>2</sub>O<sub>3</sub>, resulting in a problem of the loss of pore structure with the high regenerating temperatures [13]. ZrO<sub>2</sub> is also attractive as a metal oxide that has been utilized in a variety of catalytic CO<sub>2</sub> utilization due to its acid-basic surface and oxygen vacancy sites [14]–[16]. The appearance of the oxygen vacancy sites can promote basic sites on the surface [17]. The additions of alkaline metal oxides (Na, K) [18], [19], alkaline earth metal oxides (Ca, Mg) [20], [21], and transition metal oxides (Zr, Ni) [22], [23] raised the CO<sub>2</sub> adsorption capacity of Al<sub>2</sub>O<sub>3</sub>. Wang *et al.* reported that the Al<sub>2</sub>O<sub>3</sub> with 30% of MgO loading showed the higher CO<sub>2</sub> adsorption capacity with the

greater thermal and mechanical stability than pure Al<sub>2</sub>O<sub>3</sub> [6]. Chavez *et al.* [24] studied the influence of Al<sub>2</sub>O<sub>3</sub> content on the Al<sub>2</sub>O<sub>3</sub>-ZrO<sub>2</sub> composite. The ZrO<sub>2</sub> incorporation into Al<sub>2</sub>O<sub>3</sub> resulted in increased surface properties, protected sintering effect, and inhibited the crystallization of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> phase. Yan *et al.* [25] also studied acid-basic site property on Mg<sub>2</sub>Zr<sub>x</sub>Al<sub>1-x</sub> mixed metal oxides catalyst for the synthesis of diethyl carbonate from urea and ethanol. The catalyst is derived from layer double hydroxide that MgO and ZrO<sub>2</sub> disperse homogeneously in the Al<sub>2</sub>O<sub>3</sub> matrix. The characterization results found that acid-base sites of the catalyst facilitate the reactant adsorption mechanism. Moreover, Mg<sub>2</sub>Zr<sub>x</sub>Al<sub>1-x</sub> mixed metal oxide provided the greater basic sites than pure Al<sub>2</sub>O<sub>3</sub>.

However, there was no work studying on the surface of alumina modified with Mg-Zr mixed oxide for the CO<sub>2</sub> adsorption. The purpose of this work is to develop the CO<sub>2</sub> adsorption of the commercial Al<sub>2</sub>O<sub>3</sub> surface with Mg-Zr mixed oxide using the uncomplicated preparation method. This study hypothesizes that MgO and ZrO<sub>2</sub> should have a high potential to enhance the basicity of the Al<sub>2</sub>O<sub>3</sub> surface due to the basicity of MgO, the oxygen mobility of ZrO<sub>2</sub>, and the great interaction of Mg-Zr-Al oxide. As a result, CO<sub>2</sub> adsorption-activation of Al<sub>2</sub>O<sub>3</sub> will be then improved significantly. Moreover, the change of oxygen mobility with the CO<sub>2</sub> adsorption strength on the Mg-Zr mixed oxide modified Al<sub>2</sub>O<sub>3</sub> surface is an interesting result to be evaluated. Thus, in this study, the CO<sub>2</sub> adsorption capability of the commercial Al<sub>2</sub>O<sub>3</sub> was developed by modifying the surface with the co-functional MgO-ZrO<sub>2</sub> mixed oxide and compared to the single MgO and ZrO<sub>2</sub> oxide. MgO and ZrO<sub>2</sub>, as a metal oxide and a mixed metal oxide, were dispersed onto Al<sub>2</sub>O<sub>3</sub> via the incipient wetness impregnation method. The textural properties of commercial Al<sub>2</sub>O<sub>3</sub>, 5 wt%MgO-5 wt%MgO/Al<sub>2</sub>O<sub>3</sub>, 10 wt%MgO/Al<sub>2</sub>O<sub>3</sub>, and 10 wt%ZrO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> were investigated using N<sub>2</sub> adsorption-desorption isotherm analysis. For the surface characterization, the crystalline phases were interpreted by X-ray diffraction (XRD). The weight percentage was determined via a scanning electron microscope equipped with energy dispersive X-ray spectrometer (SEM-EDX). The oxygen mobility of all samples was evaluated by O<sub>2</sub>-temperature programmed desorption (O<sub>2</sub>-TPD). The CO<sub>2</sub> adsorption strength and capability were measured employing

CO<sub>2</sub>-temperature programmed desorption (CO<sub>2</sub>-TPD). All those properties of the MgO-ZrO<sub>2</sub> mixed oxide modified Al<sub>2</sub>O<sub>3</sub> sample were compared with other samples and discussed.

## 2 Experimental Procedure

### 2.1 Material preparation

Samples of 10 wt%MgO/Al<sub>2</sub>O<sub>3</sub>, 10 wt%ZrO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub>, and 5 wt%MgO-5 wt%ZrO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> (coded as 10M/A, 10Z/A and 5M5Z/A, respectively) were prepared by incipient wetness impregnation method. Al<sub>2</sub>O<sub>3</sub> (UNILAB) powder was impregnated with the desired amount of aqueous solutions of Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O·xH<sub>2</sub>O (98%, Acros Organics) and ZrO(NO<sub>3</sub>)<sub>2</sub>·xH<sub>2</sub>O (99.5%, Acros Organics). The wet powder was left at ambient temperature for 12 h. Thereafter, the samples were dried at 60 °C for 24 h and calcined at 600 °C for 4 h. Then, samples were pelletized and collected at the size range of 355 μm to 710 μm.

### 2.2 Characterization methods

A specific surface area, total pore volume, and average pore size diameter were calculated by Brunauer-Emmett-Teller (BET) model based on N<sub>2</sub> adsorption-desorption isotherm at -196 °C measuring with Quantachrome Autosorb-iQ-MP. The sample was degassed at 100 °C for 1 h and then at 300 °C for another 3 h until vacuum pressure was lower than 10<sup>-2</sup> kPa before the measurement.

X-ray powder diffraction (XRD) pattern was collected via Rigaku SmartLab<sup>®</sup> with Cu-Kα radiation at a scanning rate of 2°/min over the 2θ range of 2°–85°.

The morphology of the sample surface was investigated by scanning electron microscope (SEM) via FEI ESEM Quanta 450 FEG) and the elemental composition of materials were identified by energy dispersive X-ray analysis (EDX).

Temperature programmed desorption of O<sub>2</sub> (O<sub>2</sub>-TPD) studies were performed employing BELCAT BASIC<sup>®</sup> for the measurement of the oxygen mobility of samples. Prior to the measurement, helium at a flow rate of 30 mL/min was supplied for 1 h to the reactor at 200 °C to remove any contaminants from the surface of the sample. Then, the adsorption of O<sub>2</sub> was processed

at 200 °C for 1 h. Afterward, helium at 30 mL/min was supplied to the reactor again in order to purge out any O<sub>2</sub> residue and to cool down the sample to 40 °C. The O<sub>2</sub> desorption was investigated in helium flow from 40 °C to 900 °C at a heating rate of 10 °C/min and the adsorbed O<sub>2</sub> was detected by a thermal conductivity detector (TCD).

Temperature programmed desorption of CO<sub>2</sub> (CO<sub>2</sub>-TPD) studies were performed for the measurement of the basicity of samples (BELCAT BASIC<sup>®</sup>). To prepare the sample surface, the sample was heated at 200 °C for 1 h in helium flow to remove contaminants. The adsorption of CO<sub>2</sub> was operated at 40 °C with a CO<sub>2</sub> flow at 30 mL/min for 1 h, followed by a helium purge for 20 min to remove the physisorbed CO<sub>2</sub>. The CO<sub>2</sub> desorption was investigated from 40 °C to 900 °C at a heating rate of 10 °C/min. The adsorbed CO<sub>2</sub> was monitored by TCD.

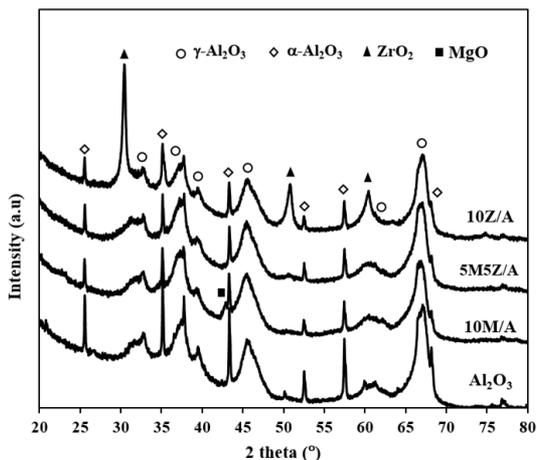
Operation of some characterization items can refer to the literature [26]–[31].

## 3 Results and Discussion

### 3.1 BET analysis

The specific surface area ( $S_{\text{BET}}$ ), total pore volume ( $V_{\text{Total}}$ ), and average pore size ( $D_{\text{pore}}$ ) of all samples are given in Table 1. As observed in Table 1, Al<sub>2</sub>O<sub>3</sub> presented  $S_{\text{BET}}$  of 95 m<sup>2</sup>/g,  $V_{\text{Total}}$  of 0.25 cm<sup>3</sup>/g, and  $D_{\text{pore}}$  of 6.3 nm. From the results, the addition of MgO and ZrO<sub>2</sub> onto Al<sub>2</sub>O<sub>3</sub> (10M/A, 5M5Z/A, and 10Z/A) caused a decrease in  $S_{\text{BET}}$  and  $V_{\text{Total}}$ . It is indicated that the Al<sub>2</sub>O<sub>3</sub> surface is covered by MgO and ZrO<sub>2</sub>.

Considering the result of 10M/A, the addition of 10 wt% MgO displayed the smaller  $S_{\text{BET}}$  (92 m<sup>2</sup>/g) with the lower  $V_{\text{Total}}$  (0.20 cm<sup>3</sup>/g) and a smaller  $D_{\text{pore}}$  (3.2 nm) than Al<sub>2</sub>O<sub>3</sub>. Meanwhile, 10Z/A showed the lowest  $S_{\text{BET}}$  (88m<sup>2</sup>/g),  $V_{\text{Total}}$  of 0.23 cm<sup>3</sup>/g, and the largest average pore size (8.1 nm). The sample of 5M5Z/A represented the textural properties between 10M/A and 10Z/A ( $S_{\text{BET}}$  of 90 m<sup>2</sup>/g,  $V_{\text{Total}}$  of 0.22 cm<sup>3</sup>/g, and  $D_{\text{pore}}$  of 7.4 nm). The different textural properties of the impregnated samples are ascribed to the particle size of metal oxide being added. As can be seen in the results, Al<sub>2</sub>O<sub>3</sub> doped ZrO<sub>2</sub> shows a higher effect of pore blocking than Al<sub>2</sub>O<sub>3</sub> doped MgO [32], [33]. It indicated that the ZrO<sub>2</sub> particles should be larger than MgO particles. The 5M5Z/A exhibited



**Figure 1:** XRD patterns of  $\text{Al}_2\text{O}_3$ , 10M/A, 5M5Z/A, and 10Z/A.

a larger  $S_{\text{BET}}$  with a smaller  $D_{\text{pore}}$  than 10Z/A. This result means that mixing MgO with  $\text{ZrO}_2$  can against the migration of  $\text{ZrO}_2$  resulting in the decrease of pore blocking effect of the  $\text{ZrO}_2$ .

**Table 1:** BET analysis of MgO and  $\text{ZrO}_2$  on  $\text{Al}_2\text{O}_3$

Sample	$S_{\text{BET}}$ ( $\text{m}^2/\text{g}$ )	$V_{\text{Total}}$ ( $\text{cm}^3/\text{g}$ )	$D_{\text{pore}}$ (nm)
$\text{Al}_2\text{O}_3$	95	0.25	6.3
10M/A	92	0.20	3.2
5M5Z/A	90	0.22	7.4
10Z/A	88	0.23	8.1

### 3.2 XRD analysis

The phase and crystalline structure of all samples were characterized via XRD analysis and diffractograms are illustrated in Figure 1. The diffractogram of  $\text{Al}_2\text{O}_3$  represents the pattern of the mixed crystalline between  $\alpha\text{-Al}_2\text{O}_3$  (at  $2\theta = 25^\circ, 35^\circ, 44^\circ, 52^\circ, 58^\circ$  and  $68^\circ$ ) and  $\gamma\text{-Al}_2\text{O}_3$  (at  $2\theta = 33^\circ, 36.5^\circ, 39^\circ, 46^\circ, 61^\circ$  and  $67^\circ$ ). It can be observed that the peak intensity of  $\text{Al}_2\text{O}_3$  was decreased when MgO was added to the surface (10M/A). However, a small diffraction peak of MgO appeared at  $2\theta$  of  $43^\circ$  indicating the dispersion of MgO on the  $\text{Al}_2\text{O}_3$  surface or MgO possibly merged with  $\text{Al}_2\text{O}_3$  to form the spinel structure ( $\text{Al}_2\text{MgO}_4$ ) [34].

Meanwhile, the characteristic peaks at  $2\theta$  of  $30^\circ, 50^\circ$ , and  $60^\circ$  of tetragonal  $\text{ZrO}_2$  (t- $\text{ZrO}_2$ ) were observed only in 10Z/A [35]. Nonetheless, the diffraction peaks of MgO and  $\text{ZrO}_2$  were not distinguished from the

sample that involve both MgO and  $\text{ZrO}_2$  (5M5Z/A). It can be implied that MgO may contribute to well dispersion of  $\text{ZrO}_2$  on the  $\text{Al}_2\text{O}_3$  surface. Moreover, the MgO diffraction peaks were rarely identified due to the sensitivity of this material and the below detectable limit of the MgO particle sizes [36].

### 3.3 SEM-EDX analysis

The surface morphology of  $\text{Al}_2\text{O}_3$ , 10M/A, 5M5Z/A, and 10Z/A all samples are displayed as SEM images in Figure 2(a)–(d) respectively. According to the SEM images, the pore structure of the  $\text{Al}_2\text{O}_3$  surface tends to be reduced after impregnating metal oxides. It can be explained by the pore blocking effect of the additional metal oxide.

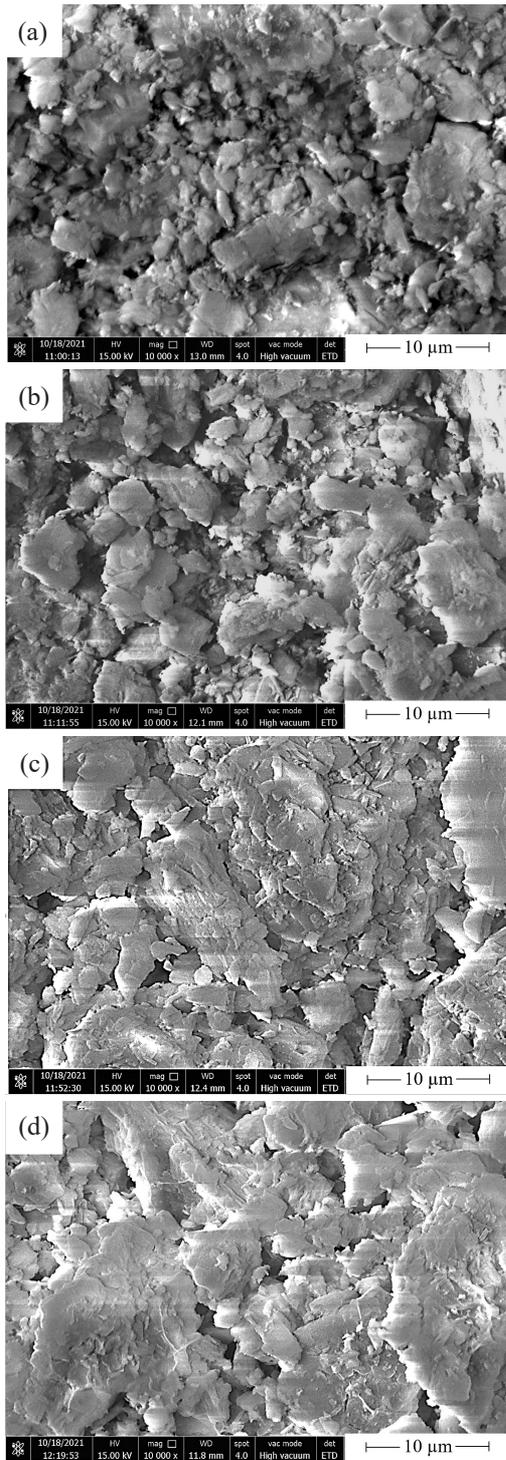
Figure 3 presents EDX analysis of all modified  $\text{Al}_2\text{O}_3$  samples. The data generated by EDX analysis consist of spectra showing peaks corresponding to the elements in the composition of the sample being analyzed. The contents of Al, Mg and Zr for each sample are revealed and reported in Table 2. The presence of Mg and Zr elements was confirmed by the EDX analysis and this result demonstrated a dispersion of MgO and  $\text{ZrO}_2$  on the  $\text{Al}_2\text{O}_3$  surface. It was observed that the percent composition of Al, Mg, and Zr are close to the desirability.

**Table 2:** EDX analysis of weight percent of Al, Mg, and Zr elements for 10M/A, 5M5Z/A, and 10Z/A

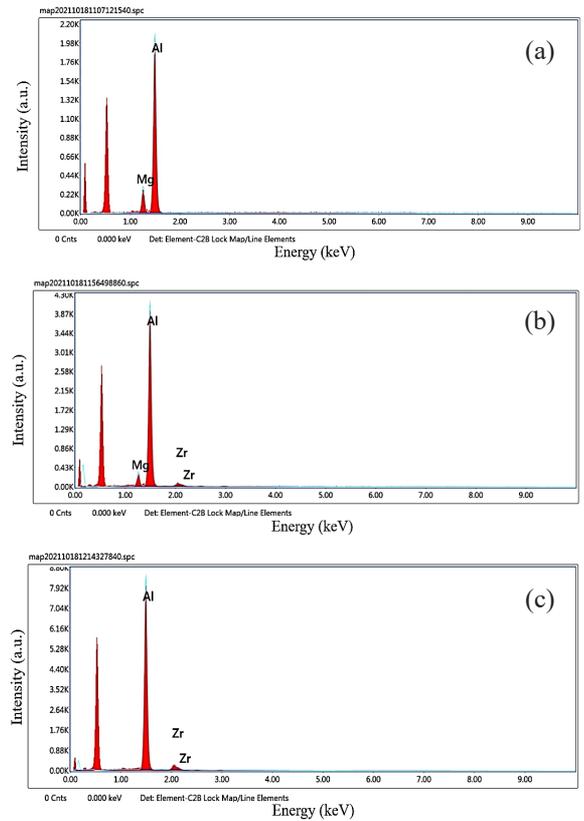
Sample	Weight Percentage (wt%) of Metal		
	Al	Mg	Zr
10M/A	89.3	10.7	-
5M5Z/A	87.8	6.2	6.0
10Z/A	89.9	-	10.1

### 3.4 $\text{O}_2$ -TPD

The oxygen mobility of the adsorbent was investigated using temperature-programmed desorption of  $\text{O}_2$  ( $\text{O}_2$ -TPD) measurement. The  $\text{O}_2$  desorption reflects the mobile oxygen species on the solid sorbent surface.  $\text{O}_2$ -TPD profiles (Figure 4) could be deconvoluted into peaks of three temperature ranges. Peaks in the range of  $50^\circ\text{C}$  to  $200^\circ\text{C}$  are the adsorbed oxygen species at the surface. Peaks that appeared at  $200^\circ\text{C}$  to  $500^\circ\text{C}$  are ascribed to the adsorbed oxygen species underneath the surface. Peaks at a temperature higher



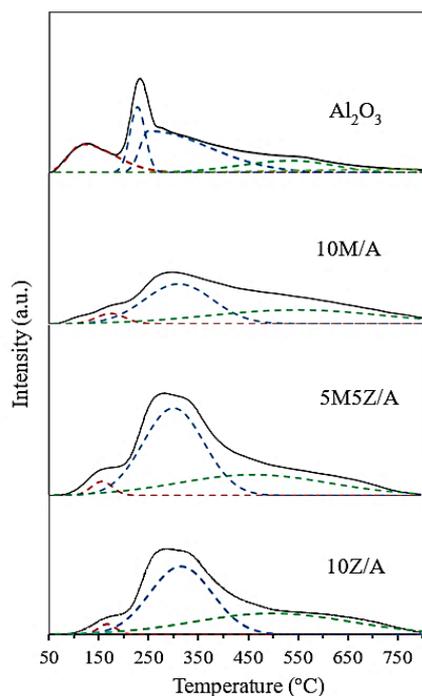
**Figure 2:** SEM images of (a) Al<sub>2</sub>O<sub>3</sub>, (b) 10M/A, (c) 5M5Z/A, and (d) 10Z/A.



**Figure 3:** EDX analysis of (a) 10M/A, (b) 5M5Z/A, and (c) 10Z/A.

than 500 °C correlate to the desorption of bulk lattice oxygen [37]–[39].

The amount of oxygen mobility of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A are reported in Table 3. The oxygen mobility of Al<sub>2</sub>O<sub>3</sub> was 1.847 mmol/g. From the results, modified Al<sub>2</sub>O<sub>3</sub> samples (10M/A, 5M5Z/A, and 10Z/A) provided higher oxygen mobility than Al<sub>2</sub>O<sub>3</sub>. 10M/A and 10Z/A gave the total oxygen vacancies at 1.970 and 2.883 mmol/g, respectively. For 5M5Z/A, the oxygen mobility increased to 3.136 mmol/g. Thus, the mixed MgO-ZrO<sub>2</sub> can greatly enhance the oxygen mobility of Al<sub>2</sub>O<sub>3</sub>. Al<sub>2</sub>O<sub>3</sub> involving ZrO<sub>2</sub> on the surface provided high oxygen mobility because ZrO<sub>2</sub> is the oxygen vacancy material. Al<sub>2</sub>O<sub>3</sub> with Mg-Zr mixed oxide on the surface showed the highest oxygen vacancy sites because Mg<sup>2+</sup> from MgO has an ionic radius of 0.65 Å which is smaller than Zr<sup>4+</sup> (0.79 Å). Therefore, Mg<sup>2+</sup> can substitute into ZrO<sub>2</sub> lattice resulting in more oxygen vacancy creation [36].



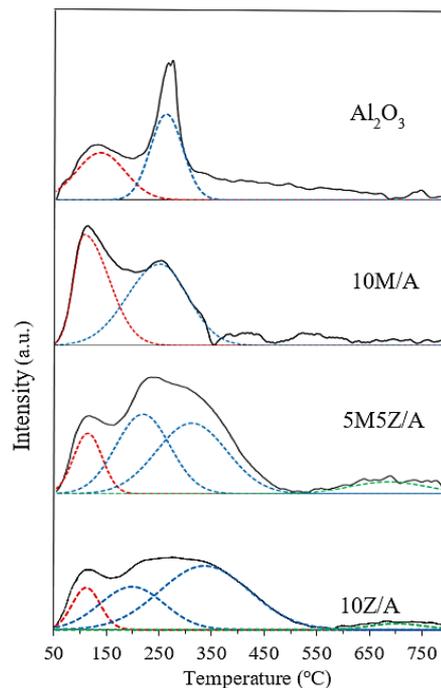
**Figure 4:** O<sub>2</sub>-TPD profiles of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A.

**Table 3:** O<sub>2</sub>-TPD profile of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A

Sample	Oxygen Mobility (mmol/g)			Total Oxygen Vacancy Site
	50–200 °C	200–500 °C	> 500 °C	
Al <sub>2</sub> O <sub>3</sub>	0.656	0.869	0.322	1.847
10M/A	0.202	0.915	0.853	1.970
5M5Z/A	0.222	2.150	0.763	3.136
10Z/A	0.271	1.882	0.730	2.883

### 3.5 CO<sub>2</sub>-TPD

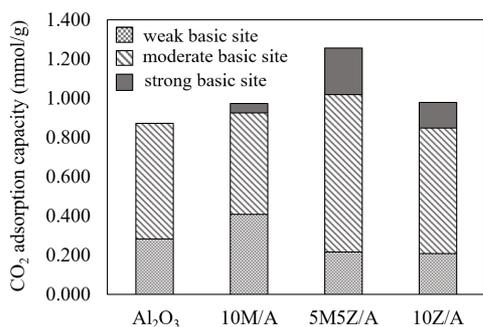
The CO<sub>2</sub>-TPD technique begins with the adsorption isotherm of CO<sub>2</sub> on the clean surface of the material. Then, flushing the physisorbed CO<sub>2</sub> by the inert gas. Afterward, the temperature increased at the constant heating rate that the chemisorbed CO<sub>2</sub> was desorbed from different basic site strengths (Figure 5). Moreover, the total CO<sub>2</sub> desorption represents the total number of basic sites as well as the CO<sub>2</sub> adsorption capacity. Figure 5 shows the CO<sub>2</sub>-TPD profiles of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A. Desorbed CO<sub>2</sub> could be attributed to adsorbed CO<sub>2</sub> on basic sites of materials. The



**Figure 5:** CO<sub>2</sub>-TPD profile of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A.

distribution of basic site strength was determined using the area under the curve fitted by Gaussian calculation. CO<sub>2</sub> desorption peaks of all profiles could be evaluated into three temperature ranges of 50–200 °C, 200–500 °C, and 500–900 °C that are assigned to the desorption of weak, moderate, and strong adsorbed CO<sub>2</sub>, respectively due to the types of basic sites on the adsorbent surface. The weak basic sites correspond to Brønsted hydroxyl groups, moderate basic sites are associated with the Lewis acid-base pairing, and strong basic sites are attributed to low-coordination surface oxygen (O<sup>2-</sup>) anions. The CO<sub>2</sub> adsorbed species are summarized in Table 4 accompanied by their structure [40]–[42].

The amount of each basic site was analyzed based on the peak area and the total amount of basic sites exhibit the CO<sub>2</sub> adsorption capacities concluding in Table 5. The CO<sub>2</sub> adsorption capacities are shown as a bar chart in Figure 6. As seen in Table 5, the adsorption of CO<sub>2</sub> on Al<sub>2</sub>O<sub>3</sub> was detected only in weak and moderate basic sites, which is the property of the commercial Al<sub>2</sub>O<sub>3</sub>. Among all samples, Al<sub>2</sub>O<sub>3</sub> has the lowest adsorption capacity of CO<sub>2</sub> (0.873 mmol/g).



**Figure 6:** CO<sub>2</sub> adsorption capacity of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A.

**Table 4:** Adsorbed CO<sub>2</sub> species on the surface of solid sorbent

Basic Site Strength	Adsorbed Species	Adsorption Site
Weak	Bicarbonate	Hydroxyl groups, Brønsted
Moderate	Bidentate Carbonate	Acid-base pairing, Lewis
Strong	Monodentate Carbonate	Low-coordination O <sup>2-</sup> , Lewis

**Table 5:** CO<sub>2</sub>-TPD profile of Al<sub>2</sub>O<sub>3</sub>, 10M/A, 5M5Z/A, and 10Z/A

Sample	Basic Sites (mmol/g)			Total/CO <sub>2</sub> ads.cap.
	Weak	Moderate	Strong	
Al <sub>2</sub> O <sub>3</sub>	0.284	0.589	-	0.873
10M/A	0.409	0.517	0.047	0.973
5M5Z/A	0.217	0.801	0.236	1.254
10Z/A	0.208	0.640	0.131	0.979

Comparisons in Table 5 and Figure 6 represents that the addition of MgO and/or ZrO<sub>2</sub> onto Al<sub>2</sub>O<sub>3</sub> improved the CO<sub>2</sub> adsorption capacity of Al<sub>2</sub>O<sub>3</sub>. For the addition of MgO (10M/A), the amount of weak and strong basic sites increased. The CO<sub>2</sub> adsorption capacity is more informative to consider the CO<sub>2</sub> adsorption performance. The CO<sub>2</sub> adsorption capacity of 10M/A is 0.973 mmol/g which increased about 11% from the CO<sub>2</sub> capacity of Al<sub>2</sub>O<sub>3</sub>. This result suggests the appearance of more basic sites that are ascribed to MgO. The additional ZrO<sub>2</sub> (10Z/A) increased the amount of moderate significantly. Then, the CO<sub>2</sub> adsorption capacity of 10Z/A increased to 0.979 mmol/g. Impregnating mixed metal oxides of MgO-ZrO<sub>2</sub> onto

the Al<sub>2</sub>O<sub>3</sub> (5M5Z/A) greatly enhanced the amount of moderate and strong basic sites and gave the highest CO<sub>2</sub> adsorption capacity. The CO<sub>2</sub> adsorption capacity of this sample was 1.254 mmol/g that increased 1.4 times higher than that of pure Al<sub>2</sub>O<sub>3</sub>.

The trend of oxygen mobility is similar to the trend of CO<sub>2</sub> adsorption capacity of all samples. It suggests that the oxygen mobility occurred by additional oxygen vacancy material plays an important role in CO<sub>2</sub> adsorption. Xin *et al.* reported that the oxygen vacancy acts as Lewis basic site and CO<sub>2</sub> is a Lewis acid [43]. This site can migrate consequence of the oxygen vacant position. CO<sub>2</sub> molecules are adsorbed on this site by filling the oxygen atom in the missing oxygen position causing in carbonate species at the surface [44]–[46]. These species will then become bidentate carbonate larger than monodentate carbonate [47]. Therefore, ZrO<sub>2</sub> incorporated with MgO prevents the migration of ZrO<sub>2</sub> and creates more oxygen vacancy sites. As a result, Mg-Zr mixed oxide modified Al<sub>2</sub>O<sub>3</sub> produces a large amount of CO<sub>2</sub> adsorption sites that show a relatively high CO<sub>2</sub> adsorption capacity.

#### 4 Conclusions

This study revealed the potential of Mg-Zr mixed oxide (MgO-ZrO<sub>2</sub>) as a co-functional material to modify the Al<sub>2</sub>O<sub>3</sub> surface for CO<sub>2</sub> adsorption. Compared to Al<sub>2</sub>O<sub>3</sub>, the impregnation of MgO, ZrO<sub>2</sub>, or MgO-ZrO<sub>2</sub> onto Al<sub>2</sub>O<sub>3</sub> enhanced the oxygen mobility and basicity of the Al<sub>2</sub>O<sub>3</sub> surface, which increases the CO<sub>2</sub> adsorption. Among all samples, MgO-ZrO<sub>2</sub> modified Al<sub>2</sub>O<sub>3</sub> provided the highest oxygen mobility of 3.136 mmol/g and showed the greatest CO<sub>2</sub> adsorption capacity of 1.254 mmol/g. It is because ZrO<sub>2</sub> incorporated with MgO create more oxygen vacancy sites than ZrO<sub>2</sub>. This vacant site can be filled by oxygen atom of a CO<sub>2</sub> molecule, which forms carbonate species at the surface and splits into bidentate or monodentate carbonates. Consequently, the Mg-Zr mixed oxide increases the number of basic sites for moderate and strong basic strength on the Al<sub>2</sub>O<sub>3</sub> surface. Thus, Mg-Zr mixed oxide modified Al<sub>2</sub>O<sub>3</sub> is a great adsorbent of CO<sub>2</sub> and can be used as a support of catalysts for CO<sub>2</sub> utilization.

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### Author Contributions

T.C.: research design, methodology, investigation, data analysis, writing an original draft; S.J.: conceptualization, research design, methodology, investigation, data analysis, writing an original draft reviewing, and editing; T.R.: methodology, and data analysis; S.T.: data analysis and editing; M.P.: conceptualization, data curation, writing-reviewing and editing, funding acquisition project administration. All authors have read and agreed to the published this version of the manuscript.

### Conflicts of Interest

The authors declare no conflict of interest.

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